

Table S1. Indices introduced in studied works

| Indices | Definition/Explanation |
|---|---|
| Clean Air Delivery Rate (CADR) | $CADR = V(k_e - k_n - k_c)$ Clean air delivery rate (CADR) in m^3/hr (ft^3/hr); V is the volume of the chamber in m^3 (ft^3); k_e is the total decay rate in h^{-1} , including both ventilation and cleaner; k_n is the natural decay rate, including only ventilation in h^{-1} ; k_c is decay rate of the pollutant concentration, reflecting loss of pollutants due to deposition or adsorption in h^{-1} (Liang & Qin, 2017). |
| Mean age of air | The average time it takes for the inlet air to reach any point of the room. Calculated using tracer decay method. $\tau = \frac{1}{C_{a0}} \int_{t_0}^{\infty} C_a(t) dt$. Uniform concentration at time t_0 is C_{a0} , the tracer C_{a0} is decaying replacing the supply air. τ is the time to clean any point in the room (W. M. Whyte et al., 2014). |
| SVE 3 | Index carried out from Fourier series low-order-components for 3D concentration distribution, agreeing to normalized age of air and normalized pollutant concentration, when uniform source of contamination is assumed (Brouns, C.; Waters, 1991; Quarini et al., 1997). |
| Figures of merit | $FM1 = \left \frac{V_L - V_S}{V} \right $ where V is the entire volume of the room, V_S is the volume of the room containing fluid with an age greater than $\frac{t_0}{2}$, and V_L is the volume of the room containing fluid with an age more than $\frac{t_0}{2}$. $FM2 = \frac{1}{2} \frac{t_0}{t_m}$ where t_m is the average age of the fluid (Quarini et al., 1997). |
| Contamination removal effectiveness | $\varepsilon_c = \frac{C_e(t_{\infty})}{C_m(t_{\infty})}$ where, C_e = Contamination concentration at exhaust, C_m = mean concentration in the room and t_{∞} = time required to obtain a stationary concentration (Lin, Hu, et al., 2010; Saidi et al., 2011). |
| Air Change Rate | $ACH = \frac{3600q_0C_0}{C_mV}$, where q_0 = airflow rate injected at pollutant source, C_0 = contaminant concentration at the source, V is room volume (Lin, Hu, et al., 2010). |
| Final efficiency | $FE = \frac{C_0}{C_m} \frac{L}{SR}$, where C_0 – concentration at the outlet, C_m – mean concentration in the room, SR – spreading radius and L is the characteristic length making this index non-dimensional. SR = the first moment of the contaminant distribution function, may be calculated as $SR = \left[\frac{\int (x-x_0)^2 C dV}{\int C dV} \right]^{0.5}$, where X_0 is the mass center of the concentration distribution function and is defined by $X_0 = \frac{\int xC dV}{\int C dV}$ (L. Zhou et al., 2017). |
| Efficiency Factor | The ratio of particle concentration in return air and average particle concentration in the room (Ljungqvist & Reinmuller, 1996). |
| Minimum air change rate | $n = \frac{(G-D)}{\{C_s[\varepsilon_v - \varepsilon_v r(1-\eta_r)] - (1-r)(1-\eta_n)\}}$ where n is the air change rate (h^{-1}), G is the rate of impurity emission in space averaged throughout the space ($count/m^3/h$), D is the rate of impurity deposition from air to surface in space averaged throughout the space, r is the ratio of recirculating air volume to supply air volume, C_s is the calculated impurity particle concentration at any time in space ($count/m^3$), η_n and η_r are the total filtration efficiency of outdoor air and recirculating air, finally ε_v is the ratio of particle concentration in return and exhaust air to average particle concentration in room (L. Zhou, Yao, et al., 2020). |
| Pump demand capacity (P_m^D) & differential pressure setpoint for the chilled water secondary and tertiary pump (P_d) | $P_d = \frac{h_t}{10.33} \times \left(1 + \frac{RM}{100}\right)$ and $p_m^d = 9.81 \times \frac{h_t \times Q \times r}{\eta}$ where the total head loss, h_t , is equal to $h_t = h_s + h_m$, main head loss for straight pipe (m), h_s , could be calculated by $h_s = \sum_{i=1}^n 10.67 \times L_i \times Q_i^{1.85} \times C_i^{-1.85} \times D_i^{-4.87}$, and h_m , minor head loss for pipe fittings and valves, is $h_m = \sum_{i=1}^n 0.5165 \times \frac{KL_i \times V^2}{g}$, finally volumetric flow rate for the i th straight pipe (m^3/s), can be calculated by $Q_i = \frac{V \times D_i^2}{k \times 6 \times 10^9}$. In these sets of equations n is the number of straight pipes in the chilled network, L_i is the length of the i th straight pipe (m), D_i is the inside diameter of the i th straight pipe (m), C_i is the roughness coefficient for the interior of the i th straight pipe, V is the flow velocity (m/s), k is the transformation coefficient, m is the number of pipe fittings and valves in the chilled network, g is the gravity acceleration of fluid, KL_i is the roughness coefficient for the i th pipe fitting or valve, Q is the volumetric flow rate in pipes beginning at the pump (m^3/s), r is the specific gravity of water, and finally η is the total pump efficiency |

Table S2. ACH Data retrieved from literature to produce Figure 3

| Reference | ACH (or average inlet air velocity) | Data Source | Reference | ACH (or average inlet air velocity) | Data Source |
|-----------------------------------|-------------------------------------|--------------|------------------------------|--|--------------|
| (West, 1924) | 20 to 60 | Review | (Bugaj & Przydrozny, 1986) | 21.5 | Experimental |
| (Yaglou et al., 1930) | 25 | Experimental | (Woods et al., 1986) | 25 | Experimental |
| (Zappfe, 1932) | 12 | Standard | (Murray et al., 1988) | 15 | Experimental |
| (Watt, 1933) | 3 | Opinion | (Sadjadi & Liu, 1991) | (0.46 m/s to 0.41m/s) | Experimental |
| (ASHVE Guide, 1943) | 8 to 15 | Standard | (Maxwell et al., 1994) | (0.30-0.33 m/s) | Numerical |
| (Blowers & Crew, 1960) | 17 | Experimental | (Campbell, 1996) | 240 to 300 | Opinion |
| (GAULIN, 1963) | 12 | Book | (Nam, 2000) | 41.9 | Numerical |
| (T.W. Keithley, W.B. Cowan, 1963) | 10 to 30 | Experimental | (Rui et al., 2008) | (0.25 m/s) | Numerical |
| (GREENBERG, 1963) | 18 to 30 | opinion | (Lin, Tung, et al., 2010b) | 70 to 139 | Experimental |
| (Goddard, 1966) | 6 to 12 | Opinion | (Y. Wang et al., 2015) | 50 | Experimental |
| (Fox, 1969) | 10 to 20 | experimental | (C. Yang et al., 2015) | 360 | Numerical |
| (Baird, 1969) | 7 | opinion | (C. Yang et al., 2015) | 288 | Numerical |
| (Clark et al., 1974) | 30 | Experimental | (Rotheudt et al., 2017) | (0.25 m/s) | Numerical |
| (Whitcher et al., 1975) | 25 | Experimental | (Khankari, 2017) | 37.5 ACH for the room and 150 ACH for the mini environment | Numerical |
| (Foord & Lidwell, 1975) | 6 | Experimental | (Loomans et al., 2019) | 6 | Numerical |
| (Manzo, 1977) | 25 | Review | (Loomans et al., 2020) | 4 | Experimental |
| (Criddle, 1978) | 30 | Experimental | (F. Y. Zhao et al., 2020) | 16-22-30 | Numerical |
| (Kundsinn et al., 1979) | 340 to 360 & 34 to 43 ACH | Experimental | (L. Zhou, Sun, et al., 2020) | 40 to 120 | Numerical |
| (Siskin, 1983) | 12 | Numerical | (Behrens et al., 2021) | 10 | Experimental |
| (Bugaj & Przydrozny, 1986) | 20 | Experimental | (Chen et al., 2022) | 15 to 25 | Numerical |

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